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Kinetic studies on the thermal dissociation of β -cyclodextrin–anisaldehyde inclusion complex

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Abstract

The stability of β -cyclodextrin–anisaldehyde (β -CDA) inclusion complex was investigated by TG and DSC. The weight loss of β -CDA ·9H₂O takes place in three stages: the dehydration occurs at 50–120°C; the dissociation of β -CDA occurs at 210–260°C; and the decomposition of β -CD begins at 280°C. The kinetics of the dissociation of β -CDA in flowing dry nitrogen was studied by means of thermogravimetry both at constant temperature and with linearly increasing temperature. The results show that the dissociation of β -CDA is dominated by a two-dimensional diffusion process (D₂). The activation energy *E* is 139.23 kJ mol⁻¹, the pre-exponential factor *A* is 1.0394 × 10¹² min⁻¹.

Keywords: Anisaldehyde; β -cyclodextrin; Inclusion complex; Kinetics

1. Introduction

 β -Cyclodextrin is an annular molecule composed of seven glucose units linked by 1,4-glucosidic bonds. Due to its annular structure, it is able to form inclusion complexes with a great variety of guest molecules as a host molecule [1, 2]. β -CD inclusion complexes with many organic compounds have been successfully utilized in the pharmaceutical and food industries. Toxicity experiments show that β -CD can be absorbed as a carbohydrate by animal and human bodies [3]. The stability and kinetic mechanism of the thermal decomposition of inclusion complexes present interesting

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problems in industrial applications. In this paper, the β -CDA inclusion complex was prepared, and the kinetics of the dissociation of this complex was studied by thermogravimetry.

2. Experimental

2.1. Preparation of the sample

 β -CD (Suzhou Gourmet Powder Factory) and anisaldehyde (Second Perfumery of Shanghai) were dissolved in water at 70°C in a 1:2 (β -CDA) molar ratio, stirred for 1.5 h at 70°C and then filtered. The white crystals were dried for 5 days at room temperature in a desiccator.

The composition of the crystals was identified by elemental analysis and TG as β -CD·C₈H₈O₂·9H₂O.

2.2. Apparatus and measurements

Thermogravimetric analysis was performed on a WRT-1 microbalance (Shanghai Balancing Instruments Factory). The analytical parameters were: sample mass, about 8 mg; atmosphere, dynamic dried nitrogen $30 \text{ cm}^3 \text{ min}^{-1}$; sample holder, $5 \text{ mm} \times 2.5 \text{ mm}$ aluminium crucible.

Differential scanning calorimetry was carried out on a CDR-1 differential scanning calorimeter (Shanghai Balancing Instruments Factory). The experimental conditions were: sample mass, about 5 mg; heating rate, 5 K min⁻¹; atmosphere, static air; reference material, Al_2O_3 .

All the thermogravimetric data (α , 0.1–0.9) were analysed on an AT-386 computer.

3. Results and discussion

3.1. The stability of the inclusion complex

Fig. 1 shows the TG and DSC curves of β -CD·C₈H₈O₂·9H₂O. The TG curve shows an 11.61% weight loss at 50–120°C, a 10.34% weight loss at 210–260°C, and a large weight loss at 280°C. The three stages correspond respectively to the dehydration, dissociation of anisaldehyde, and the decomposition of β -CD. The DSC curve has three smaller endothermic peaks at 50–110°C. These indicate that the nine water molecules are distributed in different conditions, and the necessary energy for dehydration of the internal and external water molecules is different. In addition, the oxygen atoms whose electronegativities are larger in anisaldehyde molecules can probably form stronger hydrogen bonds with the adjacent water molecules, so the dehydration process of the external water molecules is also different. The smooth endothermic peak at 210–260°C is consistent with the weight loss at 210–260°C on the TG curve. This corresponds to the escape of anisaldehyde from the β -CD cavity. The low endothermic peak indicates



Fig. 1. TG and DSC curves of β -CD · C₈H₈O₂ · 9H₂O, $\beta = 5 \text{ K min}^{-1}$.

that the attraction between β -CD and anisaldehyde results from a weak intermolecular force.

3.2. Identification of the kinetic mechanism

According to the thermal analysis results, the dissociation of β -CD·C₈H₈O₂·9H₂O takes place in three stages:

- 1. β -CD·C₈H₈O₂·9H₂O $\longrightarrow \beta$ -CD·C₈H₈O₂(s) + 9H₂O(g)
- 2. β -CD·C₈H₈O₂(s) $\longrightarrow \beta$ -CD(s) + C₈H₈O₂(g)
- 3. The decomposition of β -CD.

Our main purpose was to identify the kinetic mechanism of the second stage. First, the nine crystalline water molecules in the inclusion complex must be removed. To do this, the isothermal method was used as follows: the temperature was raised to 120° C at a heating rate of 5 K min⁻¹, and kept at this temperature for 20 min in order to dehydrate; the measurements were adjusted accordingly and then the temperature was rapidly raised to 210° C at a heating rate of 160 K min⁻¹.

The isothermal TG curve at 210°C was recorded. Using similar methods, the isothermal TG curves at 220, 230 and 240°C were recorded respectively. The non-isothermal method was used as follows: the temperature was raised to 120°C at a heating rate of 5 K min⁻¹ and kept at constant temperature for 20 min; then the heating rate was adjusted, and the non-isothermal TG curves at $\beta = 0.6, 1.2, 2.5$ and 5 K min⁻¹ were recorded respectively. The three-step judgement method [7] was used in the identification of the mechanism function, which combined an isothermal method and a linear non-isothermal method with the kinetic compensation effect.

3.3. Isothermal method

The TG curves for the isothermal weight loss of β -CD·C₈H₈O₂ are shown in Fig. 2. The kinetics of a solid-state decomposition reaction can be represented by the general equation



Fig. 2. Isothermal weight loss curves of β -CD·C₈H₈O₂: 1, 210°C; 2, 220°C; 3, 230°C; 4, 240°C.

or

$$g(\alpha) = kt \tag{2}$$

where α is the fraction of weight loss at the reaction time t, k is the rate constant, and $f(\alpha)$ and $g(\alpha)$ are functions describing the reaction mechanism. Typical theoretical model functions for solid-state reactions are shown in Table 1.

The kinetic mechanism of the weight loss process can be judged by the linear plot of the $g(\alpha)$ against time t. Taking the dissociation of β -CD · C₈H₈O₂ at 240°C as an example, Table 2 lists the linear regression results of $g(\alpha)$ versus t.

In this table, k is the rate constant, r the correlation coefficient and δ the covariance. From the evaluation of r and δ , D₁, D₂, D₃, D₄, R₃ and A₁ were selected as possible $g(\alpha)$ models.

According to the Arrhenius equation

$$k = A e^{-E/RT}$$
(3)

$$\ln k = \ln A - \frac{E}{R} \left(\frac{1}{T} \right) \tag{4}$$

 Table 1

 Kinetic models of the decomposition of solids

$g(\alpha)$	Symbol	Rate-controlling process
α^2	D ₁	One-dimensional diffusion
$\alpha + (1-\alpha) \ln (1-\alpha)$	D,	Two-dimensional diffusion
$[1-(1-\alpha)^{1/3}]^2$	D_1	Three-dimensional diffusion (Jander function)
$1 - (2/3)\alpha - (1 - \alpha)^{2/3}$	D_4	Three-dimensional diffusion (G-B function)
$\ln \left[\alpha / (1 - \alpha) \right]$	A,	Autocatalytic reaction (P-T function)
$1-(1-\alpha)^{1/n}$	R,	Phase boundary reaction, $n = 1, 2, 3$ (one-, two-, three-dimensional)
$1-(1-\alpha)^{1/n}$	A _m	Random nucleation and subsequent growth (Avrami–Erofeyev function)

Table 2 The linear regression results of the dissociation of β -CD·C₈H₈O₂ (240°C)

$g(\alpha)$	k/min ⁻¹	r	δ	$g(\alpha)$	k/min ⁻¹	r	δ
D,	2.3081×10^{-2}	0.9912	3.6064	R,	1.6604×10^{-2}	0.9861	2.5944
D,	1.9686×10^{-2}	0.9993	3.0759	RĴ	1.3448×10^{-2}	0.9926	2.1012
D_{3}	8.5414×10^{-3}	0.9934	1.3346	Å,	6.0949×10^{-2}	0.9981	9.5233
D ₄	5.4605×10^{-3}	0.9993	0.8532	Å,	2.9292×10^{-2}	0.9838	4.5769
A	9.7376×10^{-2}	0.9750	15.2151	Ă,	1.9579×10^{-2}	0.9726	3.0592
R ₁	1.9344×10^{-2}	0.9538	3.0225	Ă4	1.4750×10^{-2}	0.9656	2.3048

The related kinetic parameters of the dissociation of β -CD·C₈H₈O₂ can be obtained from a linear regression of log k versus 1/T, based on the isothermal experimental data at 210, 220, 230 and 240°C. The related E, A and r values are listed in Table 3.

3.4. Non-isothermal method

The dynamic TG curves of the thermal dissociation of β -CD·C₈H₈O₂ at different heating rates are shown in Fig. 3.

At a constant heating rate

$$\frac{\mathrm{d}\alpha}{\mathrm{d}t} = \frac{A}{\beta} \mathrm{e}^{-E/RT} f(\alpha) \tag{5}$$

$$\int \frac{\mathrm{d}\alpha}{f(\alpha)} = \frac{A}{\beta} \int \mathrm{e}^{-E/RT} \mathrm{d}T$$
(6)

$$g(\alpha) = \frac{AE}{\beta R} P(x)$$
⁽⁷⁾

where

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$$P(x) = \frac{e^{-x}}{x} \left(1 - \frac{2!}{x} + \frac{3!}{x^2} - \frac{4!}{x^3} + \dots \right), x = \frac{E}{RT} \quad \beta = \frac{dT}{dt}$$

Usually $x = E/R \gg 1$, and taking the first two approximate values

$$g(\alpha) = \frac{ART^2}{\beta E} \left(1 - \frac{2RT}{E}\right) e^{-E/RT}$$
(8)

Taking logarithms of both sides

$$\log \frac{g(\alpha)}{T^2} = \log \frac{AR}{\beta E} \left(1 - \frac{2RT}{E}\right) - \frac{E}{2.303RT}$$
(9)

From Eq. (9), it is clear that a straight line of slope -E/2.303R should result when plotting $\log(\alpha)/T^2$ against 1/T; the frequency factor A can be obtained from the intercept.

Table 3 Kinetic parameters of isothermal dissociation of β -CD·C₈H₈O₂

$g(\alpha)$	$E_{a}/(kJ mol^{-1})$	r	A	$g(\alpha)$	$E_{\rm a}/({\rm kJ\ mol^{-1}})$	r	A
D ₁	130.82	0.9920	1.2042×10^{11}	R,	132.19	0.9754	4.7555×10^{11}
D,	136.37	0.9914	1.0394×10^{12}	R,	134.46	0.9815	6.5539×10^{11}
D,	144.55	0.9975	4.4330×10^{12}	A ₁	139.69	0.9903	1.0134×10^{13}
D ₄	139.12	0.9941	3.9774×10^{12}	Å,	133.92	0.9724	1.2593×10^{12}
A.	134.49	0.9852	4.7808×10^{12}	Ă,	132.38	0.9621	5.8627×10^{11}
R ₁	131.48	0.9439	1.5463×10^{11}	A ₄	131.71	0.9557	3.7731×10^{11}



Fig. 3. Non-isothermal TG curves of β -CD · C₈H₈O₂ at a heating rate of: 1, 0.6; 2, 1.2; 3, 2.5; 4, 5 K min⁻¹.

Treating the experimental data at different heating rates by this method, it was found that the *E* and *A* values decreased with increasing heating rate. This is mainly because the sample temperature could not keep pace with the procedural temperature and the temperature range of weight loss moved to the higher region. Only when the heating rate is very low, can the recording temperature catch up with the sample temperature. Therefore, we extrapolated β to 0 K min⁻¹. Table 4 shows the results of the linear regression for the related data when extrapolating β to 0 K min⁻¹. The table also lists the *E* and *A* values obtained with different mechanism functions.

For the correct mechanism functions, the kinetic parameters obtained by the isothermal method or the non-isothermal method should be identical. Comparing the data in Table 3 with those in Table 4, and considering the proper E and A values, it is obvious that only the diffusion mechanism satisfies the requirements.

3.5. Kinetic compensation effect

In the non-isothermal thermogravimetric experiments, the E and A values will decrease with increasing heating rate. This tendency can be shown by the kinetic

$g(\alpha)$	$E_a/(kJ mol^{-1})$	log A	$g(\alpha)$	$E_{\rm a}/({\rm kJ~mol^{-1}})$	log A
D ₁	122.66	16.5703	R ,	70.96	3.9893
D,	139.23	20.2297	R ₃	76.10	4.7231
D_3	160.18	24.2071	A ₁	80.75	7.6489
D₄	138.21	18.4874	A,	40.37	-2.2211
A.		_	Ă,	23.81	-6.5126
R,	57.34	1.1129	A ₄	15.85	- 8.5157

Table 4 Kinetic parameters of the β -CD·C₈H₈O₂ thermal dissociation when $\beta \rightarrow 0$ K min⁻¹

 Table 5

 The kinetic compensation constants

$g(\alpha)$	а	b	r	$g(\alpha)$	а	b	r
D ₁	0.2698	-23.7032	0.9997	R ₃	0.2661	- 15.2784	0.9999
D,	0.2678	-23.9267	0.9998	A ₁	0.2690	- 14.7987	0.9943
D_{3}	0.2657	-25.2573	0.9996	A ₂	0.2694	-13.5060	0.9999
D₄	0.2670	-25.5401	0.9999	Ă,	0.2693	-12.8518	0.9998
R ₁	0.2699	-14.2937	0.9997	A ₄	0.2646	-12.7008	0.9997
R,	0.2666	14.8746	0.9999	-			

compensation effect [8]. Table 5 lists the compensation constants a and b for different mechanisms, together with the correlation of the linear regression.

The kinetic compensation formulae are

$$\log A = aE + b \tag{10}$$

$$E = \frac{\log A - b}{a} \tag{11}$$

$$k = A e^{-(\log A - b)/a} \tag{12}$$

where a and b are the compensation constants.

According to the compensation law, the k values can be obtained for the eleven $g(\alpha)$ models at constant temperature. Taking data at 240°C as an example, Table 6 list the k values.

The k values obtained according to the compensation law (240°C)							
$g(\alpha)$	k/min ⁻¹	$g(\alpha)$	<i>k</i> /min ⁻¹	$g(\alpha)$	<i>k</i> /min ⁻¹		
D ₁	8.6012×10^{-3}	R ₁	3.6465×10^{1}	A ₂	2.5601×10^{2}		
D,	2.1426×10^{-2}	\mathbf{R}_{2}	3.3253×10^{1}	A ₃	2.7980×10^{2}		
D,	1.2598×10^{-2}	R	2.7160×10^{1}	A ₄	1.6634×10^{2}		
D_4	1.0815×10^{-2}	A ₁	2.9253×10^2	·			

Table 6 The k values obtained according to the compensation law (240°)

Comparing data in Table 2 with those in Table 6, it is clear that only the two k values from the D_2 mechanism are equal. This confirms that the β -CD·C₈H₈O₂ thermal dissociation process is dominated by a D_2 mechanism.

4. Conclusions

 β -CD can form a stable inclusion complex with anisaldehyde, β -CD·C₈H₈O₂·9H₂O, and the stability of C₈H₈O₂ changes on being complexed by β -CD. The identification of procedural mechanism functions is one of the most difficult subjects in the study of solid thermal decompositions. The results of this study, using the three-step judgement method, show that the thermal dissociation mechanism of β -CD·C₈H₈O₂ is dominated by a two-dimensional diffusion process (D₂).

It has been confirmed that the stable energy of inclusion complexes of β -CD with weakly polar guest molecules is mainly Van der Waals energy [9, 10]. The escape of the guest molecules from the β -CD cavity is easy. The dissociation temperature far exceeds the temperature of the evaporation of anisaldehyde, and the desorption is fast. Because of the large volume of the anisaldehyde molecule, diffusion is difficult compared with that of water. Therefore the diffusion step is rate-controlling for the dissociation of β -CD · C₈H₈O₂, and the activation energy *E* and pre-exponential factor *A* are 139.23 kJ mol⁻¹ and 1.0394 × 10¹² min⁻¹ respectively.

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